

FLUID POWER DATA

PRESSURE DROPS THROUGH ORIFICES



CV FACTORS & ORIFICES

FLOW THRU ORIFICES

TO DETERMINE DESIRED ORIFICE SIZE USE THE FOLLOWING FORMULA:

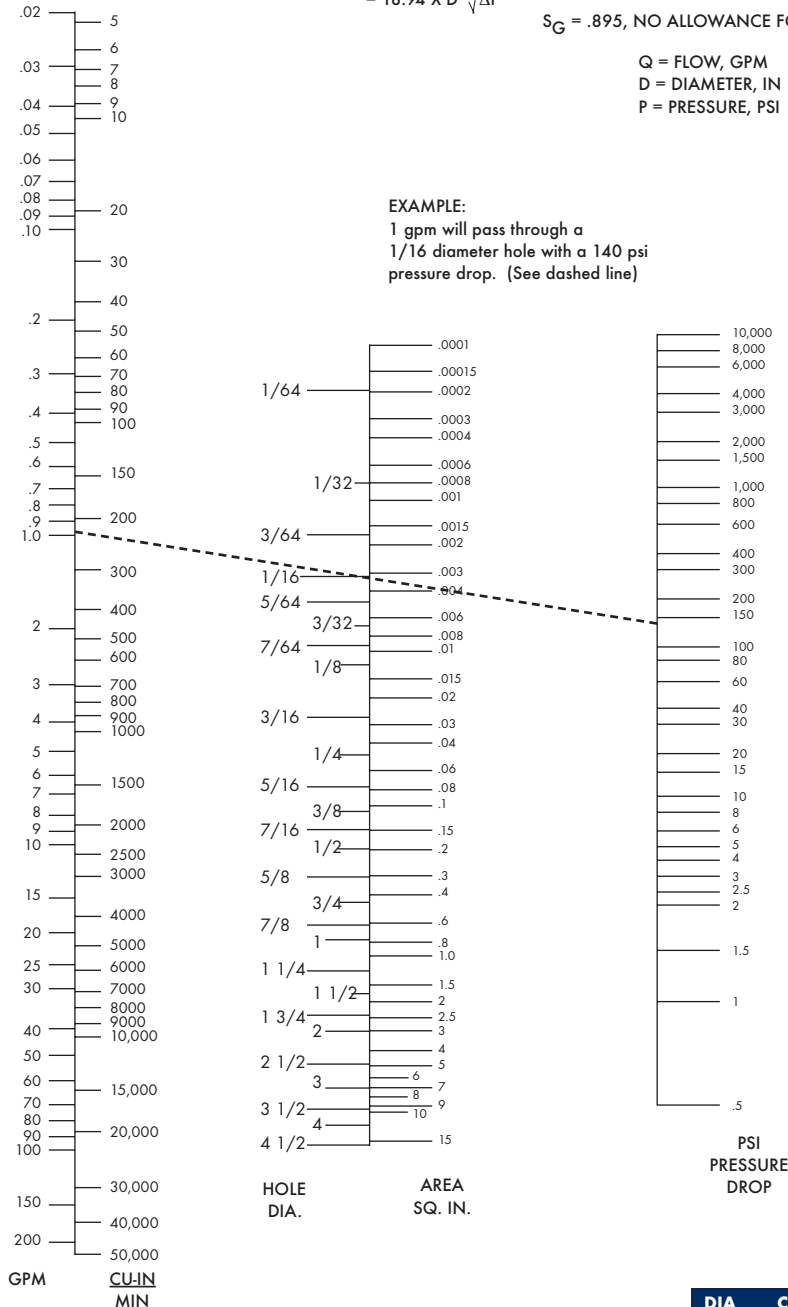
$$Q = KA\sqrt{\Delta P}$$

$$= 18.94 \times D^2 \sqrt{\Delta P}$$

WHEN C = ORIFICE COEFFICIENT .6 AND
 $S_G = .895$, NO ALLOWANCE FOR VISCOSITY CHANGE

Q = FLOW, GPM
 D = DIAMETER, IN
 P = PRESSURE, PSI

EXAMPLE:
 1 gpm will pass through a
 1/16 diameter hole with a 140 psi
 pressure drop. (See dashed line)



LIQUID FLOW THRU VALVE

$$Q = C_v \sqrt{\Delta P / S_G}$$

SHARP EDGE ORIFICE

$$Q = 29.81 (C) (I.D.)^2 \sqrt{\Delta P / S_G}$$

$$= 18.9 D^2$$

WHEN S_G IS .895
 NO ALLOWANCE FOR VISCOSITY CHANGE

C = .6 FOR SHARP EDGE
 WALL THICKNESS IS LESS THAN
 HOLE DIAMETER

C_v = GIVEN FACTOR
 I.D. = INSIDE DIA, IN
 ΔP = CHANGE IN PRESS, (PSI)
 S_G = SPECIFIC GRAVITY
 Q = FLOW, GPM, OR SCFM

C_v FACTORS FOR SHARP EDGE ORIFICES

DIA	CV	DIA	CV	DIA	CV	DIA	CV
.020	.009	.125	.35	.395	3.50	.750	12.50
.025	.014	.163	.60	.423	4.00	.875	17.30
.030	.02	.200	.90	.448	4.50	1.00	22.80
.044	.04	.212	1.00	.472	5.00	1.25	36.30
.052	.06	.250	1.50	.515	6.00	1.50	51.20
.060	.08	.300	2.00	.539	6.50	1.75	71.00
.067	.10	.333	2.50	.578	7.00	2.00	90.00
.095	.20	.375	3.13	.625	8.80	2.10	100.00

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